

Current state and ongoing development of a dynamic EAF process model

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Dynamic EAF Process Model

Comprehensive, Analytical, Fast

- All relevant phenomena
 - Heat and mass transfer, chemistry, phase changes etc.
- Complete process from tap to tap
- Applicable to different types of furnaces without adjustment of core model
- Extrapolation capability
- Fast enough for online applications









Model Overview - Development

Based on Logar et al. and Meier

- Initial publications by Logar et al. in 2011-2012
- Validation with 80MVA industrial EAF
- Further development by Meier (2013-2017)
 - o Gas phase

- Radiative heat transfer
- Automatic generation of operation chart
- Validation with 140t industrial EAF



Source: Logar, V.; Skrjanc, I.; Electric Arc Furnace Simulator; ISIJ 2012, Vol.52





Model Overview – Recent Development

Further Development after 2017

- Thermochemistry
- Radiative heat transfer
- Stability and speed

- Simulator with real-time in- and output
- Automatic generation of operation charts







Model Overview - Structure

Zones and Heat Sinks/Sources

- Zones with homogenous temperatures and compositions
- Heat transfer
 - Between zones in direct contact
 - Through radiation

Mass transfer

- Melting/Solidification
- Chemical reactions
- Injection/charging
- Chemical reactions
 - Melt/slag
 - Injection of carbon and oxygen
 - Gas zone
 - Limited heterogeneous reactions









Off-line/Validation mode

Data from industrial EAF

- Operation chart
 - Electrical power
 - Mass flows
 - 0 ...
- Charged masses, tapped mass...
- Validation
 - Continuous
 - Off-gas temperature and composition
 - Cooling water temperature
 - Electrode position
 - o Spot

- Slag and melt composition
- Melt temperature







Automatic Control Mode

Evaluation of Control Strategies

- Automatic determination of operation chart based on Meier
- Based on rules and parameters
 - Steps for input values
 - Conditions for selection of steps
 - Desired steel grade and temperature
- Different possible operation charts for the same outcome
 - Different conditions
 - Optimization







Real-Time Interaction

- In- and output through user interface
- Variable speed of the simulation
- Higher stability necessary due to more extreme possible inputs
- Possible applications in training and education
- Alternative use as soft sensor by using real-time measured data as input







Measured Data from several EAF

 Continuous and spot measurements

- Similar levels of accuracy as Meier with significantly improved speed
- Base for parameter adjustment and model validation







Case Study Results

- Case 1 to match measured profile, Case 2 to evaluated alternative oxygen source
- Same tapping temperature in all cases
- Increase in electrical and chemical energy consumption
- Increased tap-to-tap time

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 Potentially compensated by cheaper oxygen

Parameter	Case 1	Case 2
Electric energy	1	1.06
Oxygen (lance)	1.1	1.17
Oxygen (post-combustion)	1	1.06
Injected carbon	0.9	0.96
Off-gas	1.06	1.13
Natural gas	0.99	1.04
Oxygen (gas burners)	1	1.07
Total oxygen	1.07	1.14
Tap-to-tap time	0.99	1.05

Calculated performance indicators for the studied cases relative to measured values





Control of Carbon and CH₄ Injection

- Late onset of burner operation for second basket for both cases
- Longer injection and burner operation for case 2
- Similar profile of injection and burner operation with slight delay but with similar total consumption
- Case 2 increased consumption to offset N₂ content

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Conclusion

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Current status and next steps

- Comprehensive and flexible model with different operating modes
- Validation based on measured data from different EAF
- Consolidation and translation into Python for more flexibility
- Application of real-time model and model based operating strategies in industrial steel mill







Thank you for you attention

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